

Review:

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11/14/2011 (p.1)

Euler's equations after splitting:

A. ADVECTION:

$$\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} = 0$$

Solution via Semi-Lagrangian method:

$$\vec{u}(\vec{x}, t^{n+1}) = \vec{u}(\vec{x} - \Delta t u(\vec{x}, t^n), t^n)$$

subject to boundary conditions:

$$\vec{u} \cdot \vec{n} = \vec{u}_{\text{solid}} \cdot \vec{n} \text{ at any solid interface}$$

Result of this step  $\hat{u}(\vec{x}) := \vec{u}(\vec{x}, t^n)$

B. BODY FORCES (e.g. gravity)

$$\frac{\partial \vec{u}}{\partial t} = \vec{g}$$

Solution via Forward Euler:

$$\tilde{u}(\vec{x}) = \hat{u}(\vec{x}) + \Delta t \vec{g}$$

C. PRESSURE & INCOMPRESSIBILITY

$$\frac{\partial \vec{u}}{\partial t} + \frac{1}{\rho} \nabla p = 0$$

$$\nabla \cdot \vec{u} = 0$$

Solution:

→ Discretize time derivative  $\frac{\partial \tilde{u}}{\partial t}$  using forward difference

$$\frac{\tilde{u}^{(n+1)} - \tilde{u}^n}{\Delta t} + \frac{1}{\rho} \nabla p = 0$$

→ Take the divergence of these quantities

$$\nabla \cdot \frac{\tilde{u}^{(n+1)} - \nabla \cdot \tilde{u}^n}{\Delta t} + \frac{1}{\rho} \nabla \cdot (\nabla p) = 0$$

→ By the incompressibility condition, we dictate  $\nabla \cdot \tilde{u}^{(n+1)} = 0$ , thus:

$$-\frac{\nabla \cdot \tilde{u}^n}{\Delta t} + \frac{1}{\rho} \nabla \cdot (\nabla p) = 0 \Rightarrow \boxed{\Delta p = \frac{\rho}{\Delta t} \nabla \cdot \tilde{u}^n} \quad (1)$$

(where  $\nabla \cdot (\nabla p) = \Delta p$ , the Laplacian).

### Discretization

Every discrete equation stemming from (1) "lives naturally" at cell centers (indexed by whole integers  $i, j, k$ ), i.e.

$$(\Delta p)_{ijk} = \frac{\rho}{\Delta t} (\nabla \cdot \tilde{u})_{ijk} \quad \text{if } i, j, k \text{ st. } \vec{x}_{ijk} \in \mathcal{S}.$$

→ For the right-hand side we have:

$$(\nabla \cdot \tilde{u})_{ijk} = \frac{\tilde{u}_{i+\frac{1}{2},jk} - \tilde{u}_{i-\frac{1}{2},jk}}{\Delta x} + \frac{\tilde{v}_{i,j+\frac{1}{2},k} - \tilde{v}_{i,j-\frac{1}{2},k}}{\Delta y} + \frac{\tilde{w}_{ij,k+\frac{1}{2}} - \tilde{w}_{ij,k-\frac{1}{2}}}{\Delta z}$$

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(for square cells,  $\Delta x = \Delta y = \Delta z = h$ )

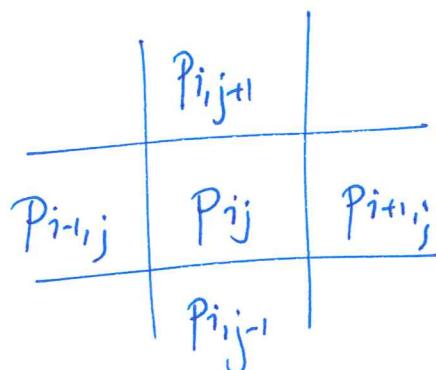
### Discretization of the Laplacian

(We demonstrate in 2D, first)

→ For cells deeply interior

$$(\Delta p)_{ij} = \frac{p_{i-1,j} + p_{i+1,j} + p_{ij-1} + p_{ij+1} - 4p_{ij}}{h^2}$$

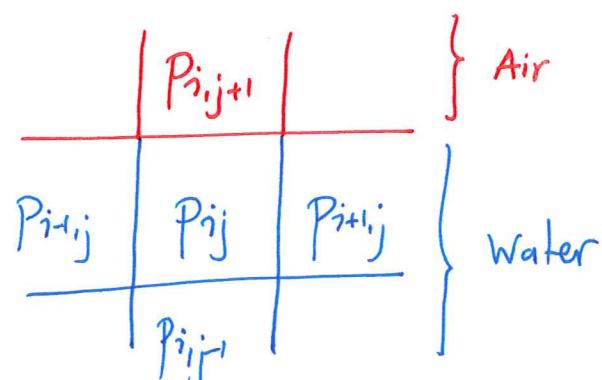
$$(\Delta p)_{ij} = f_{ij} \quad (f_{ij} := \frac{p}{\Delta t} (\nabla \cdot \tilde{u})_{ij})$$



→ For cells near the air-fluid interface

We implement the boundary condition  $p=0$  "Dirichlet" condition:

$$\frac{p_{i-1,j} + p_{i+1,j} + p_{ij-1} + p_{ij+1} - 4p_{ij}}{h^2} = f_{ij}$$



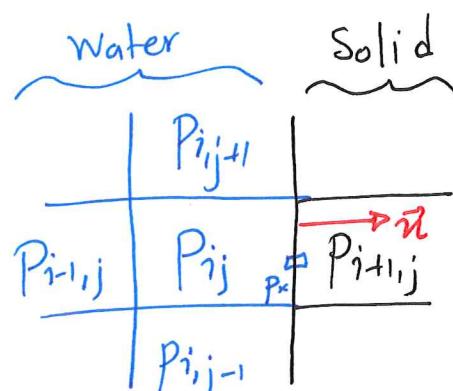
$$\frac{p_{i-1,j} + p_{i+1,j} + p_{ij-1} - 4p_{ij}}{h^2} = f_{ij}$$

→ For cells near solid boundaries

We implement the boundary condition

$$\nabla p \cdot \vec{n} = 0 \quad \text{"Neumann" condition}$$

Here,  $\vec{n} = \begin{pmatrix} 1 \\ 0 \end{pmatrix}$ . e.g.  $\nabla p \cdot \vec{n} = \begin{pmatrix} p_x \\ p_y \end{pmatrix} \cdot \begin{pmatrix} 1 \\ 0 \end{pmatrix} = p_x$



The condition  $p_x=0$  is discretized as:

$$\frac{P_{i+1,j} - P_{i,j}}{h} = 0 \rightarrow \boxed{P_{i+1,j} - P_{i,j} = 0}$$

The discrete equation becomes

$$\frac{P_{i+1,j} + P_{i,j-1} + P_{i,j+1} - 3P_{i,j} + (P_{i+1,j} - P_{i,j})}{h^2} = f_{ij}$$

Similarly, we handle the following cases:

$$\rightarrow 3D : (\Delta p)_{ijk} = \frac{P_{i+1,jk} + P_{i-1,jk} + P_{ij-1,k} + P_{ij+1,k} + P_{ij,k-1} + P_{ij,k+1} - 6P_{ijk}}{h^2}$$

$\rightarrow$  Cells neighboring more than 1 solid-water or air-water interfaces (or mixtures of the 2).

Ultimately we arrive at a system of equations

$$L \cdot p = f$$

$p$  = Vector of all pressures  
 $f$  = Vector of all right-hand-side values

We can show that:

- $\rightarrow L$  is symmetric
- $\rightarrow L$  is negative definite
- $\Rightarrow$  Thus, we can use CG to solve  $(-L)p = (-f)$  which is symmetric and **POSITIVE** definite
- (In fact, we can use CG unmodified; it works for either purely positive

or purely negative definite symmetric systems)

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Notes:

- When simulating Smoke, all Boundary conditions are Neumann; in this case 2 things happen:
- \*  $p$  is only computable up to a constant, i.e. if  $p_0(\xi)$  is a solution,  $p_0(\xi) + c$  is also a solution
  - \*  $Lp = f$  is a singular system: It has a 1-dimensional nullspace, the vector of all-constant pressures i.e. if  $p^o = (c, c, c, \dots, c)$ , then  $Lp^o = 0$
- CG can be minimally modified to handle this issue, by imposing a pre-determined average pressure  $\bar{p} = \frac{1}{N} \sum p_{ijk} = \text{const.}$
- CG can require several iterations to converge, even to elementary accuracy. As a rule of thumb if the fluid grid is of size  $N \times N \times N$ , at the bare minimum  $2N-3N$  iterations are essential, and possibly  $\sim 10N-20N$  may be required for somewhat acceptable convergence.
- \* CG can be accelerated with "preconditioning": If  $P$  is a good approximation of  $A^{-1}$  (but, cheaper to compute), preconditioning instead attempts to solve

$$Ax = b \rightarrow \underbrace{P}_{\tilde{A}} Ax = \underbrace{Pb}_{\tilde{b}} \rightarrow \tilde{A}x = \tilde{b}$$

If  $P \approx A^{-1}$ , then  $\tilde{A} \approx I$ , and CG is significantly accelerated.

Popular preconditioner : Incomplete Cholesky

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General Idea :

LU factorization  $A = L \cdot U$  ( $L/U$  are lower/upper triangular).

Problem : Even if  $A$  is sparse,  $L/U$  can be dense

Incomplete factorization :

$A \approx \tilde{L} \cdot \tilde{U}$  ( $\tilde{L}/\tilde{U}$  also triangular)

$\tilde{L}$  &  $\tilde{U}$  are only allowed to have non-zeros, where  $A$  had non-zeros in the first place

$\Rightarrow$  Trade-off between storage-complexity-accuracy.

Typical costs :

- Construction of I.C. factorization  $\approx 20x - 200x$  un-preconditioned CG iterations.
- Cost of preconditioned CG iteration  $\approx 1.5x - 5x$  un-preconditioned iterations
- Reduction in # required iterations  $\approx 5x - 20x$

### Smoke simulation

→ 2 additional physical properties :

$T$  : temperature

$s$  : concentration of smoke particles

$\Rightarrow$  Stored at cell centers, averaged when necessary.

$\Rightarrow$  Buoyancy effects

- Presence of smoke particles makes air "heavier"
- Hot air rises, cold air moves down wards

$\Rightarrow$  Replace  $\vec{g}$  (gravity) with Buoyancy term

$$\mathbf{f}_b = (0, -\alpha s + \beta(T - T_{amb}), 0)$$

$T$  = ambient temperature

$\alpha, \beta$  = constants (tune manually)

$\Rightarrow$  Temperature / Concentration Advection

Assumption: Temperature & concentration only move around, instead of explicitly diminishing (only approximate)

$$\frac{DT}{Dt} = 0 \quad \frac{Ds}{Dt} = 0$$

Use e.g. Semi-Lagrangian advection.

$\Rightarrow$  Boundary Conditions

$\Rightarrow \nabla \vec{p} \cdot \vec{n} = 0$  at any solid boundaries

$p=0$  at any container openings (allowing smoke to escape and vanish).

$\Rightarrow T = T_{object}$  at objects (can be hot!)

$\Rightarrow \vec{u} = \vec{u}_{source}$  at smoke sources

$\Rightarrow s = s_{source}$  at smoke sources ( $s=0$  inside non-source objects).

The combined effects of averaging / Semi-Lagrangian / Large time steps / Large  $h$  may lead to smoke appearing

=> Blurred, smeared out

=> Less energetic than expected (less turbulent)

=> Vortices disappearing too fast

### Remedies:

\* Vorticity confinement: We start by measuring the vorticity:  $\vec{\omega} = \nabla \times \vec{u} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ u & v & w \end{vmatrix}$

\* Determine "direction of closest vortex"

$$\vec{N} = \frac{\nabla \|\omega\|}{\|\nabla \|\omega\|\|}$$

\* Add back a "rotation force" to increase the amplitude of the twirling effect

$$\vec{f}_{\text{conf}} = \epsilon \cdot h \cdot (\vec{N} \times \vec{\omega})$$

=> As  $h \rightarrow 0$ , this extra "push" vanishes, and we get vorticity by means of better resolution.

\* Semi-Lagrangian often not accurate enough

=> Copy/Advect quantities by following curved flow lines.

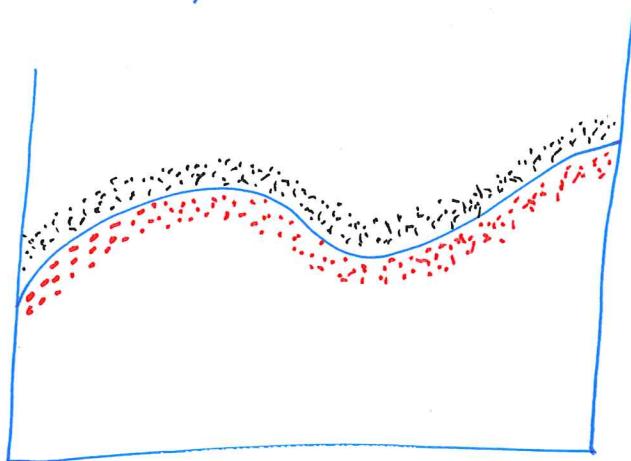
# Water simulation

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Where is the water?

A. Use marker particles



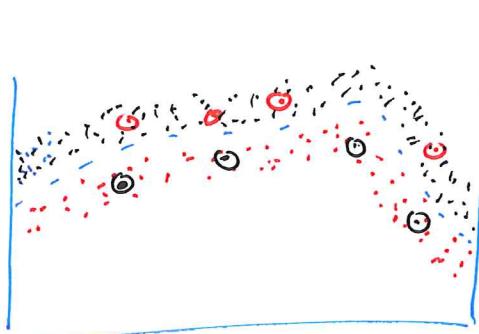
○ = Air particles

● = Water particles

Particles are moved around with the velocity field, i.e.

$$\frac{d\vec{x}}{dt} = \vec{u}(\vec{x})$$

(Note: Use at least trapezoidal rule, or another 2+ order accurate method). May need to take smaller  $dt$  for particle advection, than water simulation. Afterwards, reconstruct surface by finding interface between air/water particles

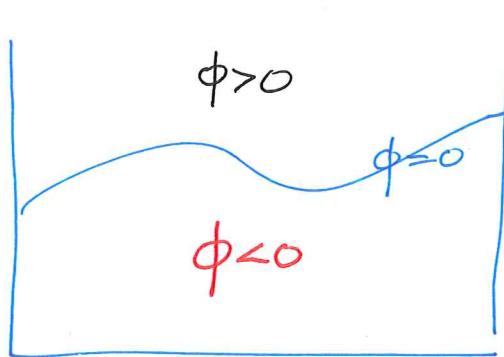


Red outliers in the air region can be rendered as spray droplets!  
(and then removed)

Black outliers in the water region can be rendered as foam/micro-bubbles

Resample as necessary!

## B. Use level-sets



Levelset values can be advected, too!  
 (Ideally, we want to move the zero levelset values, to find the new interface location, but we can advect the entire  $\phi$  field with it!)

Advection equation

$$\frac{D\phi}{Dt} = 0 \quad \text{and} \quad \boxed{\frac{\partial \phi}{\partial t} + \vec{u} \cdot \nabla \phi = 0}$$

### Issues:

→ Even if  $\phi^{(u)}(\vec{x})$  is a signed distance function, this property may be invalidated after advection!

The Fast Marching Method re-initializes the  $\phi$  function, without moving the interface  $\mathcal{I}_0 = \{x : \phi(x) = 0\}$ , such that the signed distance property is restored. (Cost =  $O(N \log N)$ ).

→ For advection algorithms, we may need  $\vec{u}$  values where it is not normally present! (i.e. in the air region). If  $\vec{x}$  is an air location we can extrapolate  $\vec{u}_{\vec{x}}(\vec{x}) = \vec{u}(\vec{x}_{\text{closest}})$  where  $\vec{x}_{\text{closest}}$  is the closest point on surface.  
 This extrapolation can be integrated into the fast marching method.